

Oxidation of ethane to ethylene and acetic acid by MoVNbO catalysts

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Abstract

The influence of niobium on the physicochemical properties of the Mo–V–O system and on its catalytic properties in the oxidation of ethane to ethylene and acetic acid is examined. Solids based on $\text{MoV}_{0.4}\text{O}_x$ and $\text{MoV}_{0.4}\text{Nb}_{0.12}\text{O}_y$ composition and calcined at 350 or 400 °C were studied by X-ray diffraction, and by laser Raman and X-ray photoelectron spectroscopies. Their reactivity during reduction and reoxidation was examined by in situ XRD and by XPS after pre-treatment. Their stability in air was evaluated by means of Raman spectroscopy during laser heating of particles. Niobium is responsible for both stabilization and nanosize of MoO_3 and $(\text{VNbMo})_5\text{O}_{14}$ crystals. The high global selectivity to ethylene and acetic acid (90–96 mol%) is related to the presence of both phases while higher activity is owed to nanoparticles. The model already proposed by Merzouki et al. (Stud. Surf. Sci. Catal., 72 (1992) 81) suggesting that MoVNbO catalysts could be made up from $(\text{VNbMo})_5\text{O}_{14}$ -type microdomains in MoO_3 matrix seems still topical.

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1. Introduction

The selective oxidation of *n*-butane to maleic anhydride has now been successfully processed, and the ammoxidation of propane is very close from industrialization. Although considerable progress has been made, the mastery of mild oxidation of paraffins to valuable chemicals remains difficult for other alkanes [1,2]. As it comes out from literature, vanadium- or molybdenum-based catalysts, which are already known for selective oxidation of unsaturated hydrocarbons, are the most useful catalysts for these tasks [3,4]. Since a long time, their combination resulting in the Mo–V–O system is known to provide good catalysts in several reactions. Among the oldest reactions, benzene oxidation to maleic anhydride [5] proceeds on a solid solution of molybdenum in V_2O_5 ($\text{V}_{1.23}\text{Mo}_{0.66}\text{O}_5$), and acrolein oxidation to acrylic acid [6,7] is carried out with phases close to V_2MoO_8 [8] ($\text{V}_9\text{Mo}_6\text{O}_{40}$) or to Mo_4O_{11} ($\text{Mo}_3\text{VO}_{11}$) [7] structure or stoichiometry. A new application was proposed in the late seventies when Thorsteinson et al.

[9] studied the oxidative dehydrogenation of ethane to ethylene. By adding Nb as a dopant of MoVO and after a careful study of the phase diagram and of the associated catalytic properties, these authors proposed that the most efficient formula was $\text{Mo}_{0.73}\text{V}_{0.18}\text{Nb}_{0.9}\text{O}_y$. Acetic acid was formed at high pressure only. Analysis by X-ray diffraction (XRD) showed the patterns of $\text{V}_9\text{Mo}_6\text{O}_{40}$ -type oxides. Solids $\text{Mo}_6\text{V}_3\text{Nb}_1$ of stoichiometry close to $\text{Mo}_{0.73}\text{V}_{0.18}\text{Nb}_{0.9}\text{O}_y$ with the same XRD pattern were also studied by Burch and Swarnakar [10]. After various tries to find other catalysts able to form directly acetic acid, Merzouki et al. [11,12], studied the preparation of $\text{Mo}_{0.73}\text{V}_{0.18}\text{Nb}_{0.09}\text{O}_y$ catalysts. When HCl or $\text{H}_2\text{C}_2\text{O}_4$ was added for solubilisation of niobium salt and ammonium vanadate, the solids resulting from heat treatment allowed acetic acid to be obtained at low temperature and atmospheric pressure. Instead of $\text{V}_9\text{Mo}_6\text{O}_{40}$ (and/or $\text{V}_6\text{Mo}_4\text{O}_{25}$), XRD patterns displayed patterns of orthorhombic MoO_3 besides, either Mo_5O_{14} or $\text{Mo}_{18}\text{O}_{52}$ when the acid added during preparation was HCl or oxalic acid, respectively. To account for these specific properties, the authors proposed a picture of MoVNbO catalysts consisting of Mo_5O_{14} -type microdomains (or of $\text{Mo}_{18}\text{O}_{52}$) in MoO_3 matrix, V and/or Nb being possibly included in these

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suboxides [11]. The properties of this system, including when modified by promoters, have been recently studied for ethane oxidative dehydrogenation [13–15] but also for production of acetic acid [16,17]. A comprehensive study of $\text{MoV}_{0.25}\text{Nb}_{0.12}\text{Pd}_{0.0005}\text{O}_y$ was led by Linke et al. [18] who suggested that the role of Pd could be to transform ethylene to acetic acid in a Wacker-like process. Promoters like Al, Fe, Cr, Ti, were proposed by Ueda and Oshihara [19] for the same reaction. Other systems of interest for production of acetic acid and/or ethylene are based on TiO_2 - [18–22] or ZrO_2 -supported vanadium oxides [22] or $\text{H}_4\text{PMo}_{11}\text{VO}_{40}$ heteropolyacid [22,23].

Catalysts like VSbO doped with W or Al for ammoxidation of propane to acrylonitrile are based on vanadium [19–26]. Multicomponent catalysts, such as those for mild oxidation of propane to acrylic acid, have flourished recently because of the versatility of the MoV system which accommodates several types of dopant [27–32]. If tungsten is generally preferred to Nb for these reactions, the Mo_5O_{14} -type oxide is often present in the system as detected by XRD and Raman spectroscopy [20,30–34], and as such it may be a key factor to relate to catalytic properties. However, the structure of other phases of the MoVXYO system, which are related to the presence of X, Y dopants, has been recently solved [35–42]. Their presence could make the difference with the MoVNbO system more active for ethane oxidation. Even though a same phase (e.g., Mo_5O_{14}) would be present, the action of W versus Nb, Al versus Te or Sb, etc., is prominent since their cationic acidity is strongly different [43,44].

In the present paper dedicated to F. Trifirò for his birthday we report on physicochemical properties of catalysts based on $\text{MoV}_{0.4}\text{O}_x$ composition, to which 0.12Nb has or not been added. To emphasize the role of Nb, their catalytic properties in the oxidation of ethane to acetic acid and ethylene are tentatively related to structural characteristics obtained by X-ray diffraction, laser Raman spectroscopy and X-ray photoelectron spectroscopies, and to reactivity by in situ methods.

2. Experimental

Catalysts $\text{MoV}_{0.4}\text{O}_x$ (MoV) and $\text{MoV}_{0.4}\text{Nb}_{0.12}\text{O}_y$ (MoVNb) were prepared according to Karim et al. [15] from ammonium paramolybdate, ammonium metavanadate, and niobium oxalate. After dessication of the mixture, the resulting powder was dried at 120 °C overnight and then calcined in air up to $T_c = 350$ °C (MoV350, MoVNb350) or 400 °C (MoV400, MoVNb400).

The specific surface area was determined by B.E.T method. XRD patterns were acquired on Huber diffractometer using Cu K α radiation. Lines were assigned to crystalline phases using the DIFFRACPlus software (Bruker) in the range $2\theta = 3$ –60°. High-temperature X-ray diffraction was carried out on a Siemens D5000 diffract-

ometer (Cu K α radiation), equipped with a HTK 1200 Anton Paar device and a PSD detector. The calibration in temperature of the heating device was checked prior to the experiments using gold powder. Samples were displayed on the sample-holder and heated at 0.06 °C/s in $\text{R}/\text{N}_2 = 20/80$ ($\text{R} = \text{H}_2, \text{C}_3\text{H}_8$ or C_2H_6). Patterns were registered at 300, 350, 400 and 450 °C (30 min at each temperature). After cooling down and sweeping by N_2 , the sample was reoxidised in $\text{O}_2/\text{N}_2 = 20/80$, and then it returned back to room temperature (RT) in the same atmosphere. Raman spectra were recorded using a Labram Infinity laser Raman spectrometer (JY-DILOR[®]). The laser intensity (Ar^+ , 514.5 nm) was reduced by various filters (<1 mW), and the data were treated by Labspec software. The spectral resolution and the accuracy in the Raman shifts are estimated to be ~ 2 cm^{-1} . A dozen particles was examined for each sample to check their homogeneity. The reactivity of samples in air was qualitatively examined by exposing powder grains to the laser beam and decreasing the intensity of filter. The same procedure was used for all samples.

XPS analyses were performed using the ESCALAB 220XL spectrometer. The powder samples were pressed in a 2 mm hole in a steel block. The Al K α monochromatized line (1486.6 eV) was used at 120 kV giving a 500 μm spot diameter in the sample. The spectrometer was operated in a constant pass energy mode ($E_{\text{pass}} = 30$ eV) for the high resolution spectra recording using the electromagnetic lens mode. There was no need of flood gun source as the samples were conducting enough. Binding energies were referenced to O1s core 530.20 eV for oxygen. During experiment the vacuum level was less than 10^{-7} Pa. Experimental quantification level and spectral simulation were obtained using the Eclipse software provided by VG Scientific. The area of Mo ($3d_{3/2}, 3d_{5/2}$), V ($2p_{3/2}$) and Nb ($3d_{3/2}, 3d_{5/2}$) peaks was measured for each sample and the surface stoichiometry was determined. Signals were deconvoluted in order to get the amount of oxidized and reduced cations. The surface oxygen stoichiometry was then calculated and compared to the two extremum values obtained from bulk stoichiometry by considering cations in their oxidized or in their reduced forms. In order to observe the effect of reduction and reoxidation on the valence of Mo, V or Nb, samples were treated by a reducing mixture (H_2/N_2 , propane/ N_2 or ethane/ $\text{N}_2 = 0.2$) for 30 min at 300 °C in the pre-treatment chamber of the VG-Escalab apparatus, and then introduced (without exposure to air) inside the vacuum chamber for acquisition of XPS spectrum. The pre-treatment temperature of 300 °C was chosen because $(\text{VNbMo})_5\text{O}_{14}$ phases are still visible by high temperature-XRD. Then the reduced samples were submitted to $\text{O}_2/\text{N}_2 = 20/80$ flow for 30 min at 300 °C in the pre-treatment chamber and examined.

The catalytic properties were measured using a conventional flow set-up, effluents being analyzed by on-line GC. The stainless-steel fixed bed reactor was placed in a tubular furnace and connected to the analysis set up. The inlet gas

mixture of propane, oxygen and nitrogen was controlled using mass flowmeters. The reactor (volume of catalyst = 3 ml) was fed with $C_2H_6/O_2/N_2 = 40/6/54$ and operated at 240–280 °C and contact time $\tau = 1$ s. Reactants and products were analysed on-line with a gas chromatograph equipped with a double detector (thermal conductivity and flame ionization) and two columns, HayeSep D 80/100 mesh, and LAC446. In these conditions, the carbon balance was met at $\pm 1\%$.

3. Results

3.1. Physicochemical analyses

3.1.1. XRD analysis

Analyses performed on fresh catalysts, with or without Nb, show distinct differences according to the calcination temperature, T_c .

Nb-free samples: The patterns of MoV350 and MoV400 display lines assigned to several phases (Fig. 1), among which orthorhombic α -MoO₃. Its amount and crystallinity increases when $T_c = 400$ °C (MoV400). It must be noted however that there is no V₉Mo₆O₄₀ nor V₂MoO₈ which are often characterized [9,10,13] in this type of sample. Most lines of α -MoO₃ are shifted to the lowest d-spacing ($2\theta \sim -0.02$ to $+0.05^\circ$) as compared to the theoretical position of α -MoO₃ lines (JCPDS 76-1003). This shift could be assigned to a modification in the crystallographic structure of α -MoO₃ by vanadium or to the formation of oxygen vacancies as in MoO_{3-x}. The Mo₅O₁₄-type structure (called θ -phase [21]) may be accounted for by its strongest reflections at $d(\text{Å})/2\theta = 3.99/22.5^\circ$ and $3.56/24.94^\circ$ which are observed in MoV350 while the two medium lines at $11.4/7.74^\circ$ and $10.2/8.67^\circ$ are present as a small “band”. The incorporation of vanadium as (V_{0.07}Mo_{0.93})₅O₁₄ [21] cannot be checked because too many lines of other phases are present. The θ -phase lines are absent in MoV400. Other phases are V_{0.12}Mo_{0.88}O_{2.94} which is a defective solid solution of V in the hexagonal form of MoO₃ (JCPDS 81-2414), and triclinic V_{0.95}Mo_{0.97}O₅ (JCPDS 77-0649), the

pattern of which is very close from that proposed for VMo₃O₁₁ [7].

Nb-containing samples: The XRD pattern of MoVNb350 (Fig. 1) is made up from several very broad reflections at $d(\text{Å})/2\theta \sim 10.8/8.1^\circ$; $4.00/22.1^\circ$; $3.28/27.1^\circ$; $2.59/34.5^\circ$; $1.99/45.38^\circ$; $1.86/48.75^\circ$. This pattern, which is similar to those observed in MoVVO catalysts [27], is characteristic of a mixture of Mo₅O₁₄-type structure and of α -MoO₃ nanocrystallites [33–35,46]. Several authors [10,33,47] identified NbVO₅ and Nb₂Mo₃O₁₁ (or 3MoO₂·Nb₂O₅, JCPDS 18-0840) in VNbMO (M = Mo, Sb, Si) catalysts for the ODH of propane. NbVO₅ is clearly absent from the pattern of MoVNb350 while (V_{0.07}Mo_{0.93})₅O₁₄ and/or (Nb_{0.09}Mo_{0.91})O_{2.80} (JCPDS 27-1310) are present (Fig. 5). The wide massif and the reflection at $(d(\text{Å})/2\theta)$ $10.92/8.08^\circ$ and $4.00/22.2^\circ$ respectively correspond to the most intense lines of these two compounds. Owing to the low amount of Nb in MoV_{0.4}Nb_{0.12}O_y formula, it would be surprising to form Nb₂Mo₃O₁₁ (or 3MoO₂·Nb₂O₅). As this pattern is very close from that of (Nb_{0.09}Mo_{0.91})O_{2.80} and because of the amorphous character of the sample, it is not easy to decide which is which. Such phases will be further mentioned as (MoVNb)₅O₁₄. After being calcined at 400 °C, samples exhibit lines of α -MoO₃ superimposed to the preceding pattern, which shows that α -MoO₃ nanoparticles already present at lower temperature have partly grown as bigger crystals.

3.1.2. Laser Raman spectroscopy (LRS)

The composition of samples on the glass holder is rather homogeneous as the same spectrum is observed, except that intensity of bands can be slightly different. The spectra of MoV and MoVNb (Fig. 2) differ at first glance by the presence of absorption bands of α -MoO₃ (bands at 996, 820, 667, 290, 160 cm⁻¹) in the former, and which are more conspicuous for MoV400 (Fig. 2). In general, Raman bands at 860–940 cm⁻¹ characterize the M'–O–M stretching mode of polycrystalline metal oxide phase, and bands at 932 and 873 cm⁻¹ are related to M–O–V phases. Bands ca. 1000 cm⁻¹ are assigned to M=O stretching mode (996 cm⁻¹). The shoulder close to 700 cm⁻¹ in MoV400 is

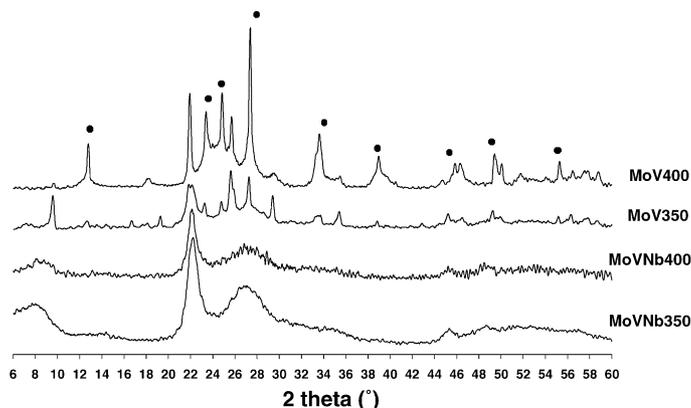


Fig. 1. XRD patterns of MoV_{0.4}O_x (MoV) and MoV_{0.4}Nb_{0.12}O_y (MoVNb) catalysts calcined at $T_c = 350$ or 400 °C (● α -MoO₃).

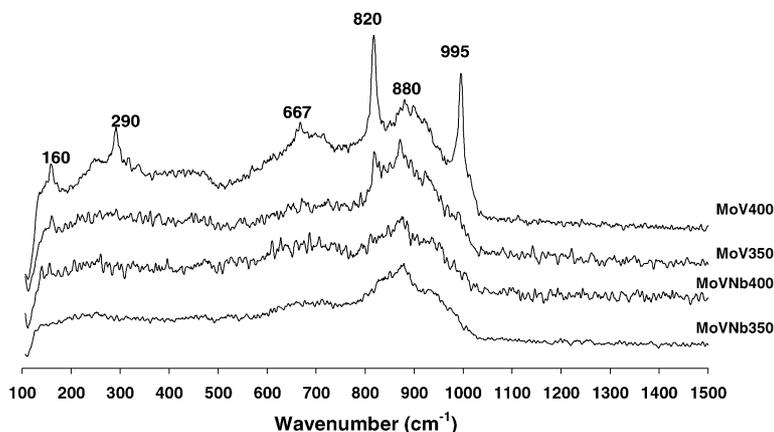


Fig. 2. Raman spectra of $\text{MoV}_{0.4}\text{O}_x$ (MoV) and $\text{MoV}_{0.4}\text{Nb}_{0.12}\text{O}_y$ (MoVNb) catalysts calcined at $T_c = 350$ or 400 °C.

assigned to V–O–V in V_2O_5 . A band with a maximum of intensity ca. $875\text{--}880\text{ cm}^{-1}$ with a shoulder ca. 920 cm^{-1} is present in both MoV and MoVNb samples. According to Mestl et al. [34,35,46], these bands are characteristic of Mo_5O_{14} -type structure. Most XRD findings are thus confirmed by LRS which shows that, (i) crystalline particles of $\alpha\text{-MoO}_3$ grow when T_c increases, (ii) Nb influences both the formation of Mo_5O_{14} -type phase and the crystallinity of the material (including MoO_3) which is poorer in its presence.

The reactivity of samples has been qualitatively estimated by using the laser beam to heat the grains on sample holder. The same definite procedure was repeated for all samples. During laser heating of MoV350, MoO_3 bands at 284 , 819 and 990 cm^{-1} are seen to grow, at the expense of bands characteristic of Mo–O–V stretching mode (~ 873 and $\sim 925\text{ cm}^{-1}$) which decrease and disappear. The same phenomenon is observed with MoV400 (Fig. 2). When Nb is present, the intensity of MoO_3 bands grows only in the case of MoVNb400 and the band structure characteristic of $(\text{MoVNb})_5\text{O}_{14}$ remains. The θ -phase is therefore stabilized by the presence of Nb.

3.1.3. X-ray photoelectron spectroscopy (XPS)

The binding energies (BE) and FWHM of Mo, V, Nb and O photopeaks are representative of Mo^{6+} , V^{5+} , Nb^{5+} and of O^{2-} in transition metal oxides (Table 1). The BE of Mo^{6+} is $232.4\text{--}232.1\text{ eV}$ and the symmetry and FWHM of Mo signal do not allow to say that Mo^{4+} or Mo^{5+} are present in samples. On the contrary, the $\text{V}2p_{3/2}$ signal is too large to account for only V^{5+} , and after deconvolution the presence of V^{4+} is

ascertained. The BE of $\text{Nb}3d_{5/2}$ is 206.7 in MoVNb350, and slightly lower (206.3 eV) after calcination at 400 °C. According to whether the oxidation state of V is $+5$ or $+4$, the bulk stoichiometry of as-prepared MoV lies between $\text{Mo}^{6+}\text{V}^{5+}_{0.4}\text{O}_4$ and $\text{Mo}^{6+}\text{V}^{4+}_{0.4}\text{O}_{3.8}$. The V/Mo ratio shows that the surface of MoV400 is enriched with Mo. This result is well correlated with the presence of MoO_3 detected by XRD and LRS. Although MoVNb400 is calcined at the same temperature, its surface is closer from stoichiometry. The presence of Nb modifies the amount of surface V^{4+} . The $\text{V}^{5+}/\text{V}^{4+}$ ratio amounts to ca. $2.7\text{--}2.8$ and $4.1\text{--}5.1$ for MoV and MoVNb, respectively, but the amount of V^{4+} versus Mo remains nearly constant in the latter.

3.2. In situ analyses

3.2.1. High temperature x-ray diffraction (HT-XRD)

Reduction: By heating MoV350 in H_2/N_2 (Fig. 3), MoO_2 is formed above 350 °C. Its main line ($2\theta = 26.0^\circ$) begins to be detectable at 400 °C, whereas the line at 22° as well as those of MoO_3 have disappeared at 450 °C. Other lines of MoO_2 ($2\theta \sim 26.0, 37.0, 41.5, 53\text{--}54^\circ$) occur above 400 °C while no line of VO_2 is observed. MoVNb350 is reduced in the same range but, that time, lines characteristic of $\text{V}_x\text{Mo}_{1-x}\text{O}_2$ ($x = 0.33$) solid solution appear at 37.8 and 54.3° besides $2\theta \sim 26.2, 36.6, 41.3, 53.4^\circ$ (Fig. 4). At 450 °C, the large lines at $2\theta \sim 22.1, 27.5, 34.8, 45.4^\circ$ assigned to $(\text{MoVNb})_5\text{O}_{14}$ and MoO_3 nanocrystallites have disappeared. It is difficult to know if Nb is incorporated or not in the $\text{V}_x\text{Mo}_{1-x}\text{O}_2$ solid solution in the absence of an

Table 1

Surface atomic ratios determined by XPS and stoichiometry of MoV and MoVNb catalysts

Catalyst	V/Mo	Nb/Mo	$\text{V}^{4+}/\text{V}_{\text{tot}}$	V^{4+}/Mo	Surface stoichiometry
MoV350 ^a	0.26	–	0.269	1.0	$\text{Mo}^{6+}\text{V}^{5+}_{0.19}\text{V}^{4+}_{0.07}\text{O}_{3.615}$
MoV400 ^a	0.50	–	0.260	0.5	$\text{Mo}^{6+}\text{V}^{5+}_{0.37}\text{V}^{4+}_{0.13}\text{O}_{4.185}$
MoVNb350 ^b	0.31	0.11	0.194	0.6	$\text{Mo}^{6+}\text{V}^{5+}_{0.25}\text{V}^{4+}_{0.06}\text{Nb}_{0.11}\text{O}_{4.02}$
MoVNb400 ^b	0.43	0.11	0.163	0.4	$\text{Mo}^{6+}\text{V}^{5+}_{0.36}\text{V}^{4+}_{0.07}\text{Nb}_{0.11}\text{O}_{4.315}$

^a Bulk stoichiometry: Between $\text{Mo}^{6+}\text{V}^{5+}_{0.4}\text{O}_4$ and $\text{Mo}^{6+}\text{V}^{4+}_{0.4}\text{O}_{3.8}$.

^b Bulk stoichiometry: Between $\text{Mo}^{6+}\text{V}^{5+}_{0.4}\text{Nb}^{5+}_{0.125}\text{O}_{4.31}$ and $\text{Mo}^{6+}\text{V}^{4+}_{0.4}\text{Nb}^{5+}_{0.125}\text{O}_{4.11}$.

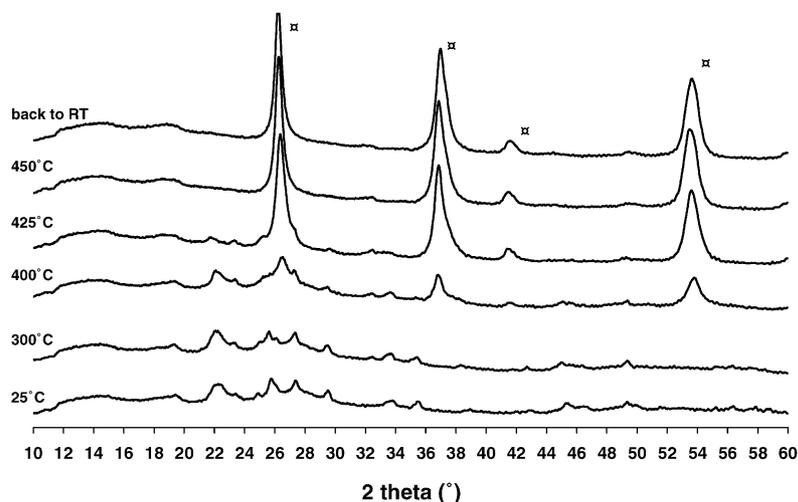


Fig. 3. XRD patterns of in situ reduction of MoV350 in H_2/N_2 atmosphere at various temperatures (x MoO_2).

internal standard. However, there is no JCPDS file of a solid solution between V and Nb or Nb and Mo.

Reoxidation: The main phases identified in patterns of MoV350 at 450 °C (Fig. 5) and after cooling are α - MoO_3 and $V_9Mo_6O_{40}$, which means that part of MoO_2 recombines with some vanadium oxide to give $V_9Mo_6O_{40}$ or V_2MoO_8 . Actually, $V_9Mo_6O_{40}$ is a solid solution of V_2MoO_8 -type, and this accounts for small d shifts and for variable intensity of some lines observed sometimes, when comparing JCPDS patterns [8]. The width of lines indicates that particles are small. After reoxidation of MoVNb350 at 450 °C (Fig. 6) the main lines of α - MoO_3 and $Mo_6V_9O_{40}/V_2MoO_8$ appear besides those (wider) at $2\theta \sim 22, 27, 45$ and 49° . These lines, which had disappeared from patterns after reduction, are assigned to $(MoVNb)_5O_{14}$ and their smaller width indicates that meanwhile the crystallinity of this phase has increased. Compared with MoV pattern after reoxidation, the occurrence of several lines assigned to crystallised

$(MoVNb)_5O_{14}$ is remarkable and undoubtedly related to the presence of Nb.

3.3. High temperature-XPS

3.3.1. Reduction by hydrogen and reoxidation by air

Only the vanadium signal is affected by reduction of samples (Fig. 7) while BEs of Mo^{6+} and of Nb^{5+} (when present) remain at 232.25 and 206.7 eV, respectively. In MoV as well as in MoVNb the deconvolution of vanadium signal yields V^{5+} and V^{4+} at 517.0 and 516.0 eV, respectively. Table 2 gathers atomic ratios and stoichiometries after reduction and after reoxidation. The bulk stoichiometry of MoV lies between $Mo^{6+}V^{5+}_{0.4}O_4$ and $Mo^{6+}V^{4+}_{0.4}O_{3.8}$ if only vanadium is reduced. By reoxidation the initial stoichiometry before experiments is not recovered and less V^{5+} are found on surface, which explains why all vanadium (IV) has not been reoxidized. During these experiments, the

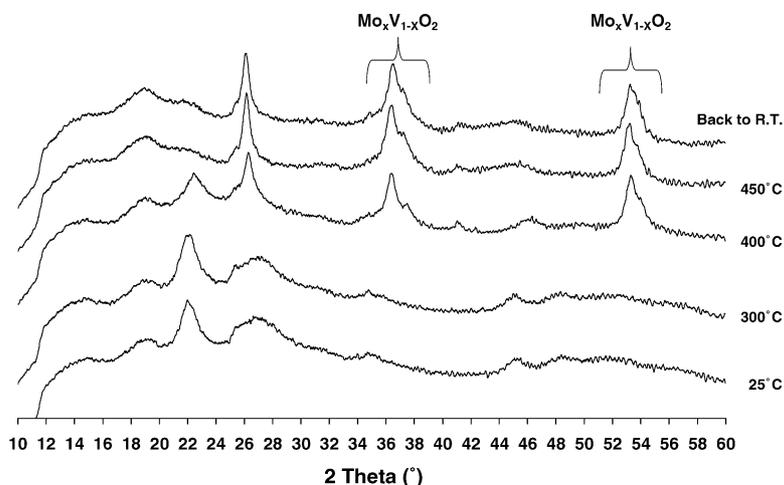


Fig. 4. XRD patterns of reduction of MoVNb350 in H_2/N_2 atmosphere at various temperatures.

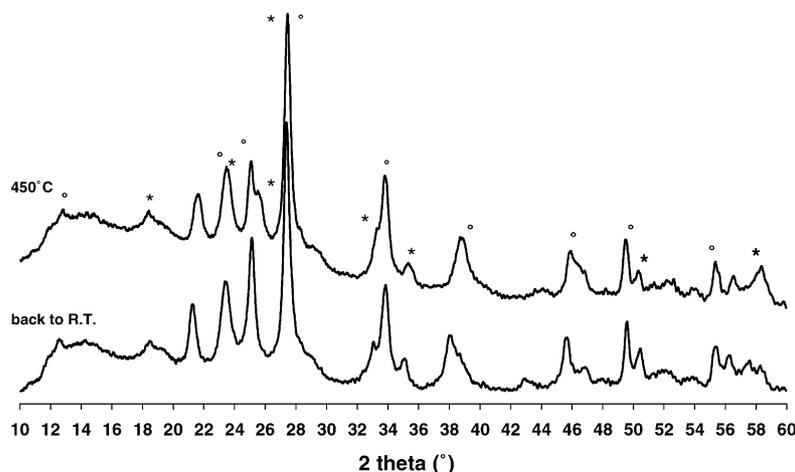


Fig. 5. XRD patterns of in situ reoxidation of the formerly reduced MoV350 at 450 °C and back to RT ($^{\circ}\alpha$ -MoO₃, *V₂MoO₈/Mo₆V₉O₄₀).

V/Mo ratio remains remarkably stable but low, which means that the surface is strongly enriched with Mo as compared to bulk. In the case of MoVNb (bulk stoichiometry between Mo⁶⁺V⁵⁺_{0.4}Nb⁵⁺_{0.125}O_{4.31} and Mo⁶⁺V⁴⁺_{0.4}Nb⁵⁺_{0.125}O_{4.11}), V/Mo is slightly greater and decreases by reduction, while Nb/Mo increases slightly. When calculating V⁴⁺/Mo, it is seen that the reduction of MoV is deeper than that of MoVNb. Therefore, the presence of Nb is responsible for decreasing the surface reducibility of vanadium and for stabilizing molybdenum. The Nb/Mo ratio is close to the 0.125 bulk value, but it increases after reduction and reoxidation. As both V/Mo and Nb/Mo increases for MoVNb as compared to MoV catalyst, this could mean that less Mo comes towards the surface in the case of MoVNb.

3.3.2. Reduction by propane or ethane and reoxidation by air

Similar reduction patterns are observed during reduction by propane or ethane. The same V/Mo ratio and the same stable Mo-rich surface of MoV are observed, and there is less Mo on surface of MoVNb. The reduction of MoV is slightly deeper than that of MoVNb (Table 3). Therefore, replacing

hydrogen by propane or ethane does not strongly modify the behavior of samples, although in the latter case, less Nb is present on surface.

3.4. Catalytic properties

Preliminary catalytic data are presented in Table 4. Catalytic experiments were deliberately performed in conditions of temperature and contact time such that oxygen was not fully converted. In the strongly reducing used conditions (C₂H₆/O₂ = 40/4), the maximum theoretical yields (referred to ethane at 100 mol% selectivity) are 20 mol% for ethylene and 6.67 mol% for acetic acid, respectively. The main products were ethylene and acetic acid, followed by CO and CO₂, with traces of acetaldehyde and formaldehyde.

When temperature of reaction T_R increases, the conversion of ethane is parallel to that of oxygen and increases while selectivity to partial oxidation products decreases. Ethylene production is systematically higher than that of acetic acid ($Y_{C_2}/Y_{AA} = 1.9$ –2.6), and carbon oxides are low. The global selectivity to ethylene and acetic acid decreases

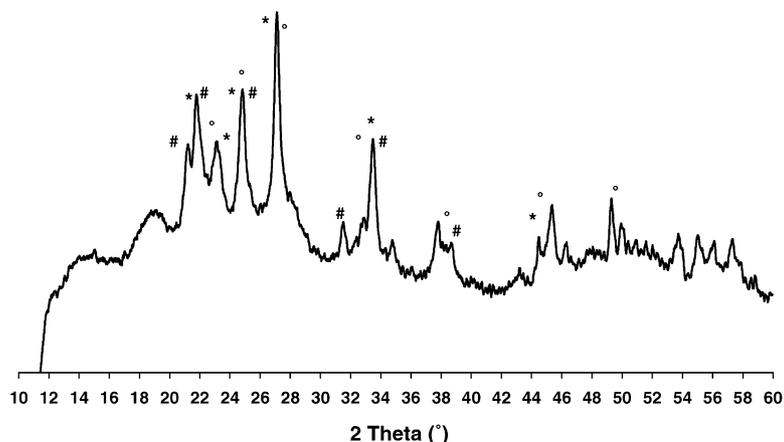


Fig. 6. XRD pattern of reoxidation of the formerly reduced MoVNb350 ($^{\circ}\alpha$ -MoO₃, *V₂MoO₈/Mo₆V₉O₄₀).

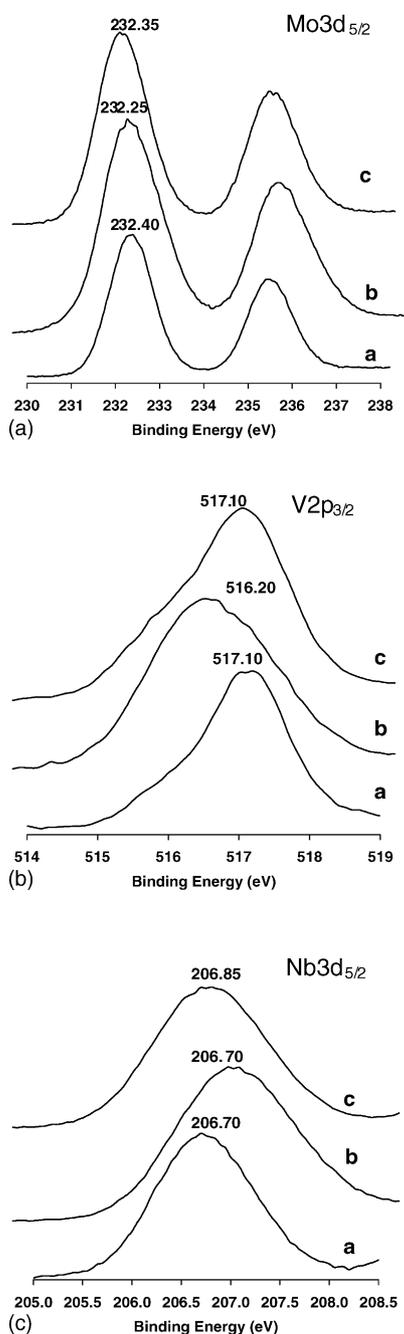


Fig. 7. XPS analysis of MoVNb350 after pretreatments; binding energy of Mo, V, Nb—(a) before reduction, (b) after reduction in H_2/N_2 and (c) after reoxidation in O_2/N_2 .

when T_R increases, and amounts to 90–96 mol% depending on samples. The main exception is MoV400, on which more carbon oxides are produced (selectivity ca. 50–28 mol%) but it is, however, the least active sample. Conversions are lower when calcination temperature T_c increases, but this effect is more noticeable in Nb-free samples. The maximum yields to ethylene and acetic acid are obtained with MoVNb350 and amount to 8.4 and 4.2 mol%, respectively. Except with MoV400, the global selectivity as well as the ethylene-to-acetic acid ratio (3.0–3.8/1) do not vary much, which means,

in first approximation, that the reaction mechanism is the same and that the main differences rely on the activity of particles.

4. Discussion

In early papers dealing with MoVO system for various applications, the presence or not of a strong XRD line ca. $d(\text{Å})/2\theta^\circ = 4.0/22$ has often been taken as an indication of good catalytic properties. Several phases may present such a line in their pattern while others do not, and most of them are gathered in Table 5. In our samples, $\theta\text{-Mo}_5\text{O}_{14}$, which belongs to the former group, has been identified, except in MoV400 where most lines belong to orthorhombic MoO_3 . The absence of $\text{V}_9\text{Mo}_6\text{O}_{40}$ (or V_2Mo_8) is noticeable in MoV and MoVNb samples while it has been found in earlier [9,10] or more recent [48] works. The presence of the recently found phases, like the orthorhombic M1 and hexagonal M2 (or those closely related to them) [36–42], whose patterns are very close from that of $\theta\text{-Mo}_5\text{O}_{14}$, is difficult to ascertain in MoVNb because of poor crystallinity. Moreover, the broad envelope ca. $2\theta = 10^\circ$ may refer to nanocrystallized $\theta\text{-Mo}_5\text{O}_{14}$ as well as $\theta\text{-MoO}_3$ (strong line at $2\theta = 9.69^\circ$) as demonstrated by Mestl et al. [46]. Therefore, we shall assume that, as confirmed by LRS, $\theta\text{-Mo}_5\text{O}_{14}$ and $\alpha\text{-MoO}_3$ constitute the common base of our catalysts, besides other phases like $\text{V}_{0.12}\text{Mo}_{0.88}\text{O}_{2.94}$ and $\text{V}_{0.95}\text{Mo}_{0.97}\text{O}_5$ in Nb-free samples. XRD and LRS show that the crystallinity of materials depends on temperature of calcination T_c , as well as on the presence/absence of Nb. Calcining MoV and MoVNb solids at 400°C results in the growing of MoO_3 crystals, which, however, are far smaller in the presence of Nb. Surface composition as determined by XPS shows that part of vanadium is reduced (V^{4+}), and that the surface is as enriched with Mo as $T_c = 400^\circ\text{C}$ and as Nb is absent.

One of the main questions to answer is the formation of solid solutions in the metastable θ -phase, which is known to be stabilized by several cations to a given extent [45]. The maximum solubility is, e.g., 11 at.% of V, 9 at.% of Nb and up to 30 at.% of W. In Nb-free catalysts θ may be stabilized as $(\text{V}_{0.07}\text{Mo}_{0.93})_5\text{O}_{14}$ but this hypothesis cannot be checked by XRD because of the presence of other oxides. Whereas V^{5+} is too small a cation, V^{4+} tolerate the 7-coordination and its ionic radius being 0.72 \AA [49] it may replace Mo in pentagonal bipyramids. The amount of V^{4+} determined by XPS (Table 1) is convenient, but to fit the oxygen stoichiometry in $\text{V}^{4+}_{0.07}\text{Mo}_{0.93}\text{O}_{2.80}$, 0.26Mo should be as Mo^{5+} , which is unlikely because of both the high symmetry and FWHM of Mo(3d) photopeak. Recently, an oxide with $\text{V}^{4+}\text{Mo}^{6+}_4\text{O}_{14}$ stoichiometry and isostructural with the θ -phase has been synthesized and characterized [30]. Owing to the initial $\text{MoV}_{0.4}\text{O}_x$ stoichiometry this oxide could also be formed, in accordance with the presence of Mo^{6+} . Using $\text{V}^{4+}/\text{V}_{\text{tot}} \approx 25\%$ close from XPS value, a rough composition

Table 2
Reduction of MoV and MoVNb catalysts by hydrogen and reoxidation by air, studied by XPS

	V/Mo	Nb/Mo	V ⁴⁺ /V _{tot}	V ⁴⁺ /Mo	Surface stoichiometry
MoV350					
Before reduction	0.26	–	0.269	1.0	Mo ⁶⁺ V ⁵⁺ _{0.19} V ⁴⁺ _{0.07} O _{3.615}
Reduction	0.26	–	0.654	2.5	Mo ⁶⁺ V ⁵⁺ _{0.09} V ⁴⁺ _{0.17} O _{3.565}
Reoxidation	0.26	–	0.385	1.5	Mo ⁶⁺ V ⁵⁺ _{0.16} V ⁴⁺ _{0.10} O _{3.60}
MoVNb350					
Before reduction	0.31	0.11	0.194	0.6	Mo ⁶⁺ V ⁵⁺ _{0.25} V ⁴⁺ _{0.06} Nb ⁵⁺ _{0.11} O _{4.02}
Reduction	0.28	0.14	0.643	2.3	Mo ⁶⁺ V ⁵⁺ _{0.10} V ⁴⁺ _{0.18} Nb ⁵⁺ _{0.14} O _{3.96}
Reoxidation	0.33	0.16	0.273	0.8	Mo ⁶⁺ V ⁵⁺ _{0.24} V ⁴⁺ _{0.09} Nb ⁵⁺ _{0.16} O _{4.18}

of MoV350 could be 0.1 V⁴⁺Mo⁶⁺₄O₁₄ + 0.3 V_{0.95}Mo_{0.97}O₅ + 0.2 MoO₃ + 0.1 V_{0.12}Mo_{0.88}O_{2.94}.

Things are different in Nb-containing catalysts. The amorphous character presented by both XRD patterns and LRS spectra of MoVNb samples is owed to the very small size of θ -Mo₅O₁₄ and α -MoO₃ crystallites [34]. Generally speaking, the thermodynamic trend exhibited by particles of amorphous materials is to reorganize and to grow in order to reach a more stable state, unless they are stabilized in another manner. Laser heating in LRS provides a means to study the stability in air. While in MoV samples the bands of MoO₃ grow as those of θ -phase disappear, in Nb-containing samples the latter remains. Niobium is undoubtedly responsible for this stabilisation and an explanation is the formation of the solid solution, as (Nb_{0.09}Mo_{0.91})O_{2.80}. Nb⁵⁺ accepts 8-coordination, and thus it may be located in pentagonal columns (r Nb⁵⁺ = 0.74 Å) [45]. Again XRD experiments do not allow to verify the hypothesis, that time because of the amorphous character of XRD patterns and LRS spectra. However, another, though indirect, proof that V and/or Nb could enter the θ -phase lattice is provided by in situ HT-XRD experiments on samples calcined at 350 °C. The reduction of the Nb-free sample by hydrogen shows that MoO₂ is formed while no line accounts for the presence of vanadium oxide, and the reoxidation does not give back the θ -phase but V₉Mo₆O₄₀ and MoO₃. On the contrary, the same experiments on MoVNb show that, not only the reduction yields the (MoV)O₂ solid solution, but also the reoxidation gives back (VNbMo)₅O₁₄ (besides V₉Mo₆O₄₀ and α -MoO₃). Moreover, meanwhile the crystallinity of (VNbMo)₅O₁₄ has increased. If more Mo is

stabilized by formation of (VNbMo)₅O₁₄, it is normal that XPS shows less ‘free’ Mo (probably as MoO₃) on surface than in MoV, and that Nb tends to be more present among the bulk.

‘In situ’ XPS experiments also provide informations (Tables 2 and 3). The temperature of pretreatment (300 °C) was chosen in accordance with T_R of catalytic experiments. No formation of reduced molybdenum (Mo⁵⁺, Mo⁴⁺) was observed, in accordance with HT-XRD since, at this temperature, no MoO₂ was yet formed. The reduction affects vanadium in similar amounts (V⁴⁺/V_{tot} = 0.59–0.67) whatever the reducing agent, and at first sight less V is reduced in the presence of Nb (V⁴⁺/V_{tot} = 0.59–0.64 for MoVNb versus 0.62–0.67 for MoV). However, by calculating $\Delta = (V_{R}^{4+} - V_0^{4+})/V_0^{4+}$, where V₀⁴⁺ and V_R⁴⁺ relate to the initial and after reduction amounts respectively, it is seen that $\Delta = 2.1$ – 2.3 for MoVNb versus 1.3 – 1.5 for MoV. In other words, Nb favors the reduction of V, which thus may enter the θ -phase more easily, as shown by the presence of Mo_{1-x}V_xO₂ in HT-XRD. By reoxidation at 300 °C, the initial mean valence state of V is not recovered. This may be due to the fact that Mo came onto the surface during reduction, the result being that some V specie are hidden and not reoxidized [46]. This trend is less marked in the presence of Nb.

Previous work on the MoVNbO system by one of the authors [11] has demonstrated that the step of solubilization of ammonium metavanadate and of niobium oxide is prominent to avoid the presence of phases like V₉Mo₆O₄₀, and that heat treatment in inert atmosphere ensures the formation of reduced Mo oxides. There are two ways for

Table 3
Reduction of MoV and MoVNb catalysts by propane and by ethane, and reoxidation by air, studied by XPS

	Propane				Ethane			
	V/Mo	Nb/Mo	V ⁴⁺ /V _{tot}	V ⁴⁺ /Mo	V/Mo	Nb/Mo	V ⁴⁺ /V _{tot}	V ⁴⁺ /Mo
MoV350								
Before reduction	0.26	–	0.269	1.0	0.26	–	0.269	1.0
Reduction	0.26	–	0.615	2.4	0.27	–	0.673	2.5
Reoxidation	0.26	–	0.423	1.6	0.28	–	0.357	1.3
MoVNb350								
Before reduction	0.31	0.11	0.194	0.6	0.31	0.11	0.194	0.6
Reduction	0.27	0.13	0.593	2.2	0.33	0.09	0.607	1.8
Reoxidation	0.29	0.12	0.414	1.4	0.34	0.09	0.295	0.9

Table 4

Surface area and catalytic performance (mol%) of MoV and MoVNb catalysts in the oxidation of ethane to ethylene and acetic acid

	S_{BET} (m ² g ⁻¹)	Temperature (°C)	Conv. C ₂ H ₆	Conv. O ₂	Sel. AA	Sel. C ₂ H ₄	Sel. AA + C ₂	Sel. CO	Sel. CO ₂
Mo ₁ V _{0.398} ^a MoV350	34	240	3.5	26.0	27.0	66.0	93.0	3.0	4.0
		260	8.0	55.1	29.0	61.0	90.0	5.0	5.0
		280	11.0	77.4	30.0	57.0	87.0	6.0	7.0
Mo ₁ V _{0.398} ^a MoV400	21	240	1.5	11.2	19.0	53.0	72.0	12.0	16.0
		260	2.0	19.4	17.0	46.0	63.0	14.5	23.0
		280	2.5	33.8	16.0	34.0	50.0	21.0	29.0
Mo ₁ V _{0.398} Nb _{0.125} ^a MoVNb350	26	240	6.5	33.5	27.0	69.0	96.0	1.5	2.3
		260	11.0	62.9	29.0	66.0	95.0	2.3	3.0
		280	13.5	88.2	31.0	62.0	93.0	3.0	4.0
Mo ₁ V _{0.398} Nb _{0.125} ^a MoVNb400	24	240	6.0	33.4	27.0	69.0	96.0	2.0	2.0
		260	9.5	63.5	26.0	66.0	92.0	4.0	4.0
		280	12.0	92.9	25.0	65.0	90.0	5.0	5.0

^a Sample composition: AA: acetic acid; C₂: C₂H₄.

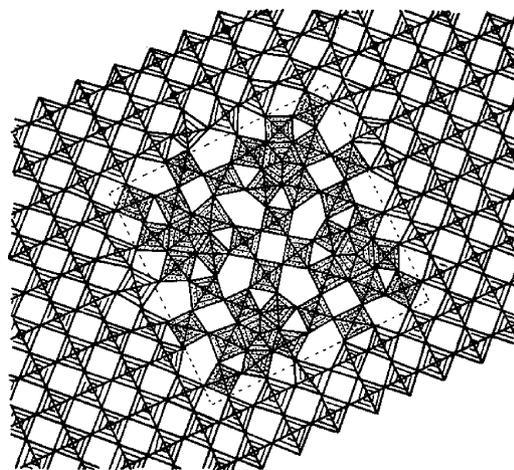
Table 5

Main Mo- and MoV-based oxides (Mo/V > 1:1) exhibiting (or not) a line $d = 4 \text{ \AA}$ in their XRD pattern

Phase	Mo/V	Crystal structure	Parameters	JCPDS N ^o	Line at $ca. 4 \text{ \AA}$
V _{0.95} Mo _{0.97} O ₅	1.02	Triclinic	$a = 6.334 \text{ \AA}$, $\alpha = 90.00^\circ$, $b = 4.046 \text{ \AA}$, $\beta = 7.30^\circ$, $c = 3.725 \text{ \AA}$, $\gamma = 90.50^\circ$	77-0649	Yes
VMo ₃ O ₁₁	3.0	Hexagonal	$a = b = 4.00 \text{ \AA}$, $c = 3.76 \text{ \AA}$, $\beta = 120^\circ$	[6,7]	Yes
V _{0.13} Mo _{0.87} O _{2.935}	6.70	Hexagonal	$a = b = 10.592 \text{ \AA}$, $c = 3.699 \text{ \AA}$, $\beta = 120^\circ$	48-0766	No
V _{0.12} Mo _{0.88} O _{2.94}	7.33	Hexagonal	$a = b = 10.593 \text{ \AA}$, $c = 3.694 \text{ \AA}$, $\beta = 120^\circ$	81-2414	No
V _x Mo _{1-x} O _{2.80} $0 \leq x \leq 1.0$	0–15	Tetragonal (Mo ₅ O ₁₄ -type)	Variable	31-1437	Yes
h-MoO ₃	–	Hexagonal	$a = b = 10.531 \text{ \AA}$, $c = 14.876 \text{ \AA}$, $\beta = 120^\circ$	21-0569	No
Mo ₄ O ₁₁	–	Orthorhombic	$a = 24.54 \text{ \AA}$, $b = 5.457 \text{ \AA}$, $c = 6.752 \text{ \AA}$	84-0687	Yes

MoO₃ to be partly reduced. The first one, which is common to V, Nb, Ti, W, oxides, is by means of crystallographic shear planes and gives rise to the so-called Magnéli phases. This mechanism has even been shown to proceed in the case of the reduction of α - or β -VOPO₄ to (VO)₂P₂O₇, catalysts of mild oxidation of 1-butene or *n*-butane to maleic anhydride [50,51]. The second mechanism is responsible for the formation of pentagonal columns by extensive edge-sharing between polyhedra [45], and is common to W, Te, etc., oxides as well as, e.g., uranium molybdates [52]. In the examined conditions [11], oxalic acid was leading to the formation of Mo₁₈O₅₂-type oxide, while hydrochloric acid favored the formation of θ -Mo₅O₁₄. The stabilization by V and/or Nb was also assumed via their partial insertion in these phases. In the first case, the formation of acetic acid was concomitant to that of ethylene and observed at atmospheric pressure and at temperature as low as 200 °C ($S_{\text{AA}} = 42$, $S_{\text{C}_2} = 45$ mol%), acetic acid decreasing while ethylene increased ($S_{\text{AA}} = 2$, $S_{\text{C}_2} = 80$ mol% at 350 °C). In the second case, acetic acid was obtained at 200 °C with very high selectivity (ca. 100 mol%) and then it decreased while ethylene increased ($S_{\text{AA}} = 20$, $S_{\text{C}_2} = 55$ mol% at 350 °C). In the present work, and although a detailed catalytic study has not yet been conducted, the behavior of all samples but MoV400 is similar: ethylene and acetic acid are obtained together, the former being in higher amounts, and only the conversion of ethane differs. In a short range of temperature

(40 °C), the global selectivity amounts to 89–96 mol%. These findings must be related to the same system where θ -(VNbMo)₅O₁₄ and MoO₃ are present, their crystalline state being mainly related to their catalytic activity. Werner et al. [30] have emphasized the role of the ‘glassy nanocrystalline state’ of such material in catalysis. On the contrary, if crystals of MoO₃ are too large, and because they naturally exhibit mostly {0 1 0} faces, the production of CO_x is high [53]. This is the case of MoV400 catalyst which

Fig. 8. Model of coherent interfaces between θ -(VNbMo)₅O₁₄ and α -MoO₃; after [11].

is characterized by the lowest surface area, ethylene conversion and selectivity to ethylene and acetic acid. Therefore, high conversion is related to the presence of nanocrystallites (XRD, LRS), and high selectivity is related to the least amount of ‘free’ MoO₃ found on surface, that is for MoVNb350.

The relative role of these two phases is a different story which is related to synergistic effects [54,55]. Several examples of efficient catalysts containing ‘free’ MoO₃ may be found in literature, and in most cases the latter is associated with cobalt molybdate, e.g., for maleic anhydride formation from n-butane [55,56], or nickel molybdates for propane oxidative dehydrogenation [57–59]. The model of (Mo,V,Nb)₅O₁₄ microdomains in α-MoO₃ proposed in 1991 [11] (Fig. 8) and which emphasized the role of coherent interfaces, seems still topical.

5. Conclusions

The influence of niobium on the properties of MoV_{0.4}-based catalysts is plural. Provided the preparation and the heat treatment of precursor is convenient so as to avoid the formation of Mo₆V₉O₄₀, Nb first allows the formation and the stabilization of θ-Mo₅O₁₄ system. Niobium probably enters this lattice but also it seems to favor the incorporation of some vanadium (may be as VMo₄O₁₄), as indirectly shown by the formation of Mo_{1-x}V_xO₂ during in situ XRD reduction of MoVNb samples. The disordering of the θ structure could result from the formation of (VNbMo)₅O₁₄ solid solution. Secondly, during preparation and/or heat treatment, Nb favors the formation of MoO₃ nanoparticles which, however, are more thermally stable as seen by laser heating (LRS) and less prone to move toward the surface (XPS). At this stage, it is difficult to say more about the possible presence of oxides structurally related to M1 or M2. Restricting ourselves to catalysts for ethane oxidation, these oxides are more easily observed in the absence of Nb, e.g., Mo₆V₂M, (M = Al, Sb, Te) provided they are hydrothermally prepared from Anderson heteropolymolybdates [19]. With our samples, the catalytic performance in strongly demanding conditions (C₂/O₂ = 10), and particularly the high global selectivity (90–96 mol%) as well as the ethylene-to-acetic acid ratio, is nearly the same every time both θ-(VNbMo)₅O₁₄ and MoO₃ nanoparticles are present. Therefore, we suggest that synergistic effects between these structurally related oxides are responsible for the high values of selectivity, as well as for the modified reactivity of MoVNb in non-catalytic conditions.

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